

Economics of Local Materials as Base Fluids in The Formulation of an Oil Based Mud

By

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ABSTRACT

The use of drilling fluid is an important aspect in drilling operations as its critical to ensure a safe and productive oil or/ and gas well. In the bid to protect the environment and reduce environmental pollution resulting from drilling activities while using the No. 2 diesel, it is necessary to search for an alternative that will be suitable, locally available, easily affordable vegetable oils which is environmentally friendly and non-toxic as base fluid. This study is aimed at investigating the properties and economics analysis of the use of non-toxic, biodegradable locally obtainable oil from the palm kernel seed (Oil X) and coconut (Oil Y) as base fluid in the formulation of an Oil Based Mud. The rheological and filtration properties of the mud samples were evaluated using the API Recommended Standard, while the economics analysis was performed using the Net Present Value (NPV) and discounted profit to investment ratio (DPI) models. The results of the rheological, filtration and physiochemical properties for both X-OBM and Y-OBM, showed the possibility of the use of oil X or Y as base fluid as against No. 2 diesel. The result from the NPV model showed that the use of oil X or Y provided a higher NPV compared to those of No. 2 diesel mud even though the cost of No. 2 diesel was lower than those of X and Y oils. Also the discounted profit to investment ratio (DPI) was also better for mud formulated from the vegetable oil muds. Although the initial cost of formulating mud samples using oil X or Y compared to No. 2 diesel Oil Base Muds (OBM) seems higher, consideration of their fire capacity resistance, nonimpact on the environment and the cost of disposal of OBM the application of vegetable oil X or Y is more viable than No. 2 diesel in the industry

Key words: Coconut oil (Oil Y), Palm Kernel seed (Oil X), Diesel, Net Present Value, Discounted Profit to Investment Ratio

1.0 Introduction

The Nigerian oil and gas industry have in the past few years witnessed a changing terrain with the advent of the Local Content Act. The local content act encourages the substitution of imported materials with locally obtainable replacement. Generally, Water Based Mud (WBM) and Oil Based Mud (OBM) are the most widely used drilling fluid types in the oil and gas industry. Oil based systems were developed and introduced in the 1960s to help address several drilling problems most notably swelling or sloughing of clays upon reaction with WBMs. But the need to protect the environment and reduce environmental pollution resulting from the use of No. 2 diesel as base fluid in OBM has led to the quest for an environmentally friendly suitable substitute for diesel. The alternative to diesel fuels must be technically and environmentally acceptable and economically viable. As a result, vegetable oils shall be considered as viable alternatives to diesel, although it has high viscosity due to large molecular weight and bulky molecular structure.¹ Also the use of vegetable oils will help strengthen the relationship and interaction between the agricultural and energy sector.

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¹ Anastopoulos, G.; Zannikou, Y.; Stournas, S.; Kalligeros, S. (2009), Transesterification of vegetable oils with ethanol and characterization of the key fuel properties of ethyl esters. *Energies* 2, 362–376.

A lot of effort has been made by researchers since 1991 to date on the use of vegetable oil as base fluid in the formulation of an environmentally friendly Oil Base Muds. Yassin et al² and Ismail, A.R.³, these researchers used palm oil as the base fluid and determined the toxicity of the use of palm oil but Yassin et al further examined the rheological and filtration properties of the mud samples. Although Yassin et al, noted that the oil had a high plastic viscosity, but they all noted that the oil had low toxicity, high flash point and good emulsion stability. Sanchez et al,⁴ in their work evaluated the toxicity and biodegradability of the oil-base drilling fluids formulated from the use mineral oil and palm oil against that of diesel, their results show that mineral and palm tree oil based fluids are not toxic while diesel showed high toxicity levels In 2010, Ogunrinde and Dosumu⁵ in their study used both palm oil and groundnut oil as base fluid in an OBM. They determined the rheological properties and the toxicity of the mud sample. From their results they concluded that the use of both oil as base fluid should be encouraged. Researchers now are looking into the use of synthetic oils as being more environmentally friendly than the conventional diesel or mineral oil-based mud.

Fadairo et al,⁶ using jatropha and canola oil as base fluid developed an ANN model for predicting the down hole mud density of these mud sample. The No. 2 diesel was also determined and used as control. Their results showed that both jatropha and canola oil possessed a great prospect. In 2012, Adesina et al⁷ used jatropha and rapeseed oil while Apeleke et al⁸ used rapeseed oil alone as base fluids in the formulation of an OBM. They all carried out the rheological and filtration properties test and concluded that these oils were good suitable for No. 2 diesel. Ogeleka et al⁹ carried out a study to evaluate the toxic effect of diesel OBM using brackish water shrimps obtained from Abua in Rivers state as the test species for the study. The water shrimps were exposed to varying concentrations of drilling fluid waste and it was observed that the mortality rate was dependent on the drilling fluid waste concentration.

Anawe et al¹⁰ investigated the use of jatropha OBM and groundnut OBM as alternatives to diesel OBM. The rheological properties of all three muds were determined at different temperatures. Jatropha OBM was observed to possess the highest viscosity and density of all the three mud

² Yassin, A.M; Kamis, and Abdullahi, M.O. (1991): Palm Oil Diesel as a Base Fluid In Formulating Oil Based Drilling Fluid . SPE Paper23001

³ Ismail, A.R. (2011): Managing the Environmentally Friendly Drilling Fluid in Petroleum Industry. The 2nd International Conference on Disaster Management, Surabaya, Indonesia, 3- 5 May.

⁴ Sáchez, G; León, N, Esclapés, M; Galindo, I; Martínez, A; Bruzual, J; Siegert, I (1999) *Environmentally Safe Oil-Based Fluids for Drilling Activities*” SPE 52739, Paper presented at SPE/EPA Exploration and Production Environmental Conference held in Austin, Texas, 28 February–3 March 1999.

⁵ Dosumu A and Ogunrinde, J.O (2010): Development of Environmentally Friendly Oil Based Using Palm Oil and Groundnut Oil SPE Paper 140729.

⁶ Fadairo, A., Ameloko, A., Adeyemi, G., Ogidigbo, E. and Airende, O. (2012). *Environmental impact evaluation of a safe drilling mud.*

⁷ Adesina F. David, O and Olugbenga, F. (2013): Investigating the Cutting Carrying Capacity and the Effect of Drilled Cutting on Rheological Properties of Jatropha Oil Based Mud Paper SPE 167551.

⁹ Ogeleka, D.F. and Tudararo-Aherobo, L.E. (2013). *Assessment of the toxic effects of oil-based drilling mud (drilling waste) on brackish water shrimp (palaemonetes africanus).*

¹⁰ Paul Apeye Lucky Anawe, Vincent Enon Efevbokhan, A. A. Ayoola and Otuekong Akpanobong. “Investigating alternatives to diesel in oil based drilling mud formulation in the oil industry” *Journal of Environment and Earth Sciences*, 2014. 4 (14). pp. 70-77. ISSN 2224-3216

samples. Akintola et al¹¹ examined the filtration properties of using melon, groundnut soybean and palm oil as base fluid. Their result showed the ranking in order of better and effective filtration properties as shown melon, groundnut soybean and palm oil. Agwu et al¹² carried out a comparative study on diesel and soybean oil as base fluid for an OBM. they observed that diesel OBM lost more filtrate during the filtration test compared with that of soybean OBM and were able to conclude that the soybean OBM would be better suited as drilling fluid compared to diesel OBM.

The mud samples density was obtained using the pressured mud balance. The rheological properties were determine using the Fann 35A and calculated using the equations 1.0 – 3.0 while the API Filter press was used to obtain the 30mins water loss.

$$Av = \frac{\theta_{600}}{2.0} \quad 1.0$$

$$Pv = \theta_{600} - \theta_{300} \quad 2.0$$

$$Yp = \theta_{300} - Pv \quad 3.0$$

Economic analysis is carried out to compare and contrast between projects or alternatives in order to choose which is most cost effective, viable and produces the most benefits. The analysis was carried out using the Net Present Value and Profitability Index by applying the equations 4.0 and 5.0, respectively.

$$NPV = -I + \frac{CF_t}{(1+i)^t} \quad 4.0$$

$$DPI = \sum_0^t DCF_t * \frac{1}{I} = \frac{NPV}{I} \quad 5.0$$

2.0 MATERIALS AND METHODOLOGY

2.1 Materials: No. diesel oil, palm oil, coconut oil, and organophilic clay. The additives used for formulating of the mud were obtained from MI-Swaco Limited, Port-Harcourt, Rivers State. The chemicals used were of analytical grade.

2.2 Apparatus: These include: Weighing scale, mud balance, sample containers, mixer, measuring cylinders, viscometer, thermometer, mixer, hydrometer, Pensky-Martens closed cup flash tester, Kehler model k-16270, Capillary Viscometer (Herzog GmbH MP480), pycnometer, beakers, Soxhlet Extractor and API Filter press

2.3 Extraction of Oil from Palm Kernel Seeds and Coconuts

The palm kernel seeds were obtained from a farm in Ondo state while coconuts were purchased from a local market in Ibadan, Oyo State. The extraction of the oils was carried out using the Soxhlet apparatus n-haxane was used as solvent.

2.4 Determination of Physicochemical Properties of the Extracted Oils

¹¹ Akintola, S. Oriji, A.B. and Momodu, M. (2014): Analysis of Filtration Properties of Locally Sourced Base Oil For The Formulation of Oil Based Drilling Fluids. *Scientia Africana*, Vol 13 No 1 Pp 171 -177

¹² Agwu, O.E., Anietie, O.N. and Udoh, F.D. (2015). *A comparative study of diesel oil and soybean oil as oil-based drilling mud.*

To know if the base fluid will have the desired properties, its physicochemical properties were determined, four properties density, pour point and flash point and kinetic viscosity were measured in the department of Petroleum Engineering Laboratory, University of Ibadan:

- a) **Density and Specific Gravity:** The density of the extracted oils was determined using a (50ml). pycnometer and a weighing balance. The density was calculated using the equation 6.0 while the specific gravity was determined using a hydrometer

$$\text{Density, } \rho = \frac{\text{Mass (m)}}{\text{Volume (v)}} \quad 6.0$$

- b) **Pour Point:** The ASTM D97 method was used to determine the pour points

c) **Flash Point:** The Pensky-Martens closed cup flash tester, Kehler model k-16270 was used to obtain the flash point

- d) **Kinematic Viscosity:** The Kinematic Viscosity was determined using the Capillary Viscometer

2.5 Formulation of Mud Sample

A 9 ppg mud was formulated as presented in the Table 1.0 using the different base oils (Oil X, oil Y and diesel oil) with an oil water ratio of 70:30 was used.

Table 1.0: Formulated 9.0 ppg Mud Sample with the Different Oil as Base Fluid

Material	Quantity	Concentration (field units)	Mixing Order	Mixing Time (mins.)
Base Oil (X, Y and Diesel)	218.3	ppb	1	
VG Plus	6.00	ppb	2	12
Lime	8.00	ppb	3	3
Novamul	8.00	ppb	4	10
NaCl	5.00			
Water	88.62	ppb	5	10
Versatrol	8.00	ppb	6	5
Barite	86.06	ppb	7	5

2.6 Economic Analysis

For the economic analysis, a well drilled at Area AB1 foothills in the Alberta region of Canada was used as case study. The depth data and costs were obtained from the Petroleum Services Association of Canada (PSAC) 2015 well costs summary brochure. The casing length(ft) and hole size (inches) for surface, intermediate and production casing for the well drilled into an oil formation with a Total depth of 14,763 feet using a 6.625 inches drill pipe is shown in the Table 2.0. The well has a porosity of 30% and an assumed initial daily well production of 500 barrels per day. The mud cost is made up of the cost of the oil, cost of treatment of cuttings before disposal and cost of transportation and disposal of cuttings. It is assumed that stained cuttings would require little to no treatment cost.

Table 2.0: Casing Length(ft) and Hole Size (Inches) for Surface, Intermediate and Production Casing

Type of Casing	Casing Length(ft)	Hole Size (Inches)
Surface	1,969	16.00
Intermediate	8,990	13.375
Production	3,805	8.5

An economic model Is prepared using the well costs and calculated mud costs if the well was drilled using X, Y or D OBM. The required mud volume and volume of cuttings generated were determined using the equations 7.0 and 8.0

$$\text{Required Mud Volume} = \frac{d^2}{1029.4} * D \quad 7.0$$

$$\text{Volume of cuttings generated} = \frac{d^2 + (1 - \phi)}{1029.4} * D \quad 8.0$$

Cost Requirements

Well cost excluding mud cost = \$ 14,337,890.00

Treatment cost = \$50 per barrel; Haulage and disposal cost = \$20 per barrel

The equation 9.0 is used to obtain the mud cost requirement for the different base fluids

Mud cost requirements =

$$\left(\text{oil cost in } \frac{\$}{\text{bbl}} * \text{reqd. oil volume} \right) + \text{cuttings volume} * (\text{treatment cost} + \text{disposal cost}) \quad 9.0$$

The following steps were used in the preparation of the economic model:

- The mud and rock cuttings volume that would be required to drill through the production and intermediate zones only assuming the surface zone would be drilled with a water-based mud was determined. Also, the mud costs inclusive of cuttings treatment and disposal costs that would be required to drill through intermediate and production zones was calculated.
- An NPV model using revenue obtained from a 12years production forecast using exponential decline curve analysis was prepared and calculate other economic decision-making parameters.

3.0 Results and Discussion

a) Oil Recovery Breakdown

Mass of unbroken seed	= 5.36 kg
Mass of broken seed	= 3.78 kg
Mass of water expelled from seed	= 5.36 – 3.78 = 1.58 kg
Mass of shell	= 1.048 kg
Mass of extracted oil, Y	= 543.66 g
Weight of nuts X	= 2115.29 grams

Weight of extracted oil X	= 747.35 grams
Dry weight of pycnometer	= 19.31 grams
Viscometer size and constant	= 200 and 0.1, respectively
Weight of pycnometer filled with oil Y and X	= 65.31 and 64.81 grams, respectively.
The dynamic and kinematic viscosity is calculated using equations 7.0 and 8.0	
Dynamic viscosity= density (ρ) * flow time (t)*viscometer constant(K)	7.0
Kinematic viscosity = flow time (t)*viscometer constant(K)	8.0

b) Physiochemical Properties of Oil X and Y: The results of the physiochemical properties are shown in Table (2).

Table 2.0: Physiochemical Properties of Oil X and Y

	Specific Gravity	Dynamic Viscosity (cp)	Kinematic Viscosity (cp)	Pour point (°C)	Flash point (°C)
Oil X	0.91	32.5	29.45	20	225
Oil Y	0.92	13.1	12.05	20	242

2) Density of Mud Sample:

The density of the mud sample was measured at temperature of 30°C and the results presented in the Table 3.0. It can be observed that No.2 diesel OBM had the least density followed by X OBM and then Y OBM. The increase in mud density follows the trend of the density of the base oils this shows that the density of the base oil plays a role in the overall density of the mud system. The mud density result also shows that X OBM and Y oil OBM would do a good job in controlling formation pressures and prevention of influx of formation fluids into the wellbore.

Table 3.0: Mud Density(ppg) at 30°C

Mud Sample	Density(ppg) @30°C
XOBM	9.31
YOBM	9.30
DOBM	8.76

3) Rheological Properties

The mud samples rheological properties were determined by applying the equations 1.0 – 3.0. From the plot of the plastic viscosity against temperature, Figures 1.0, it is observed that the plastic viscosity of X and Y OBMs, increases before it starts to decrease as temperature increase. but that of diesel OBM decreased steadily with increasing temperatures. At lower temperatures, the X OBM and Y OBM, had values of plastic viscosities higher than the recommended values. This can be attributed to the high value of the specific gravity of their base fluid Overall, a decrease in plastic viscosity with increasing temperatures can be observed for the three mud systems but from the three mud systems, DOBM has the least plastic viscosity followed by X OBM and Y OBM.

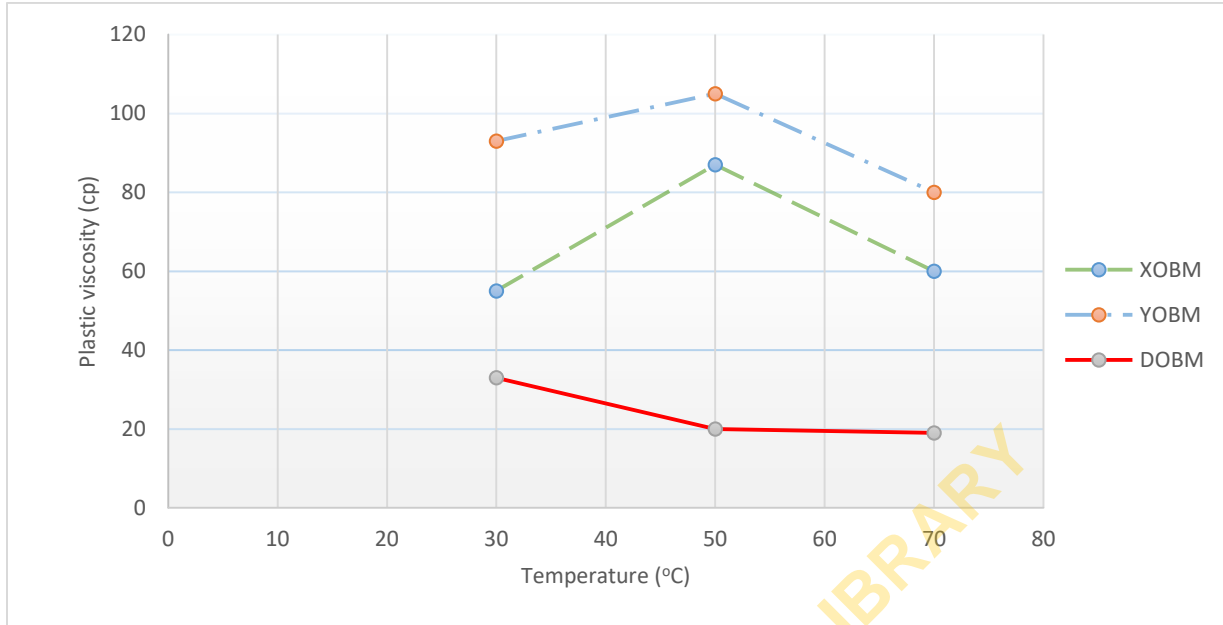


Figure 1.0: Plastic viscosity (cp) against Temperature (°C) for X OBM, Y OBM and DOBM

From the Figure 2.0 it can be observed that the yield point decreases with increasing temperatures for the three mud systems. A decrease in yield point values with increasing temperature is as a result of the effect of temperature on the intermolecular bonds between the molecules of the mud. High

temperatures weaken the bonds and as a result, at higher temperatures, less stress would be needed to break the bonds and initiate flow. At surface temperatures, the X OBM had the highest yield point followed by the Y OBM and then the DOBM. At temperatures above 40°C, the yield point of the X oil continues to decrease drastically. This shows that at higher temperatures, the X OBM can perform like the diesel OBM based on yield point values.

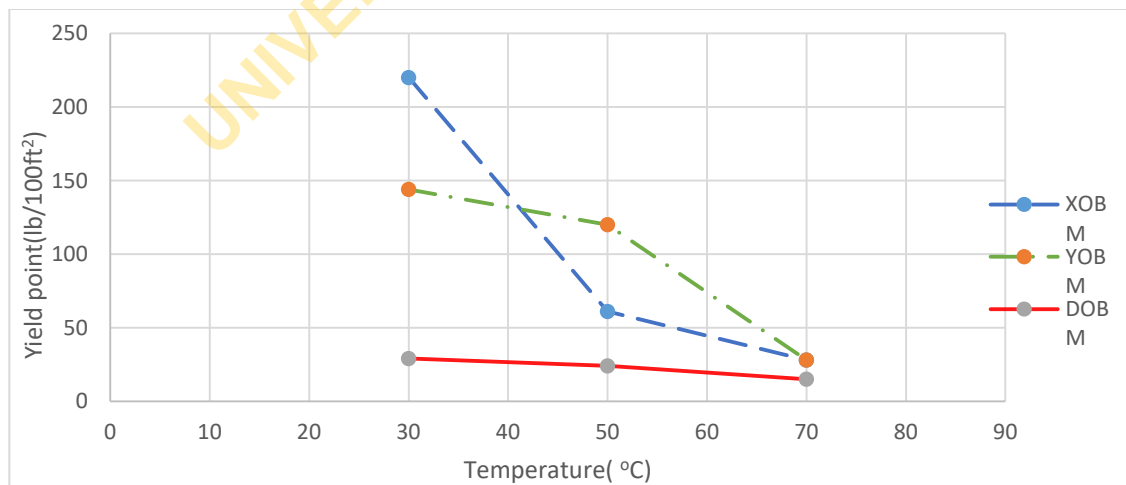


Figure 2.0: Yield point against Temperature (°C) for X OBM, Y OBM and DOBM

From Figure 3.0 the gel strengths for all the mud systems decrease with increasing temperature. Decreasing gel strength with increasing temperature is the effect of temperature on the intermolecular bonds within the mud molecules as the bonds tend to weaken as temperatures increase. At surface temperatures, X OBM has the highest gel strength and diesel OBM has the least gel strength. However, gel strength values of X OBM decrease drastically with increasing temperature and equal the gel strength value of diesel OBM at 67°C.

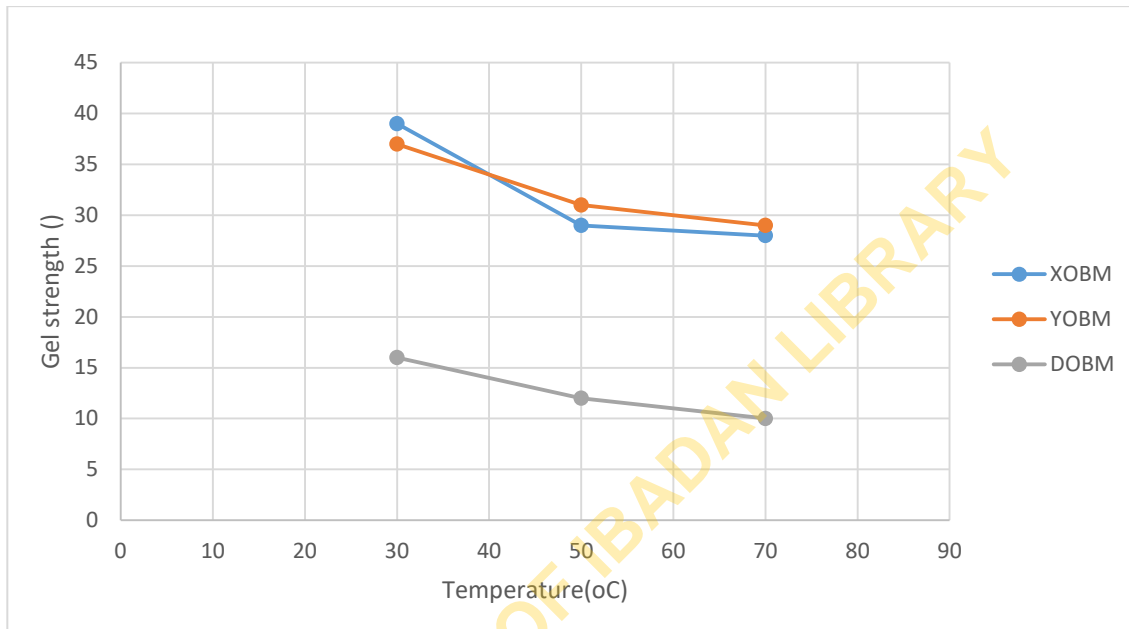


Figure 3.0: Gel strength against Temperature (°C) for X OBM, Y OBM and DOBM

FILTRATION

From the Figure 4.0, Y OBM possesses the highest fluid loss values followed by diesel OBM and X OBM. This means that Y OBM has a higher tendency to form a porous and thick filter cake compared.

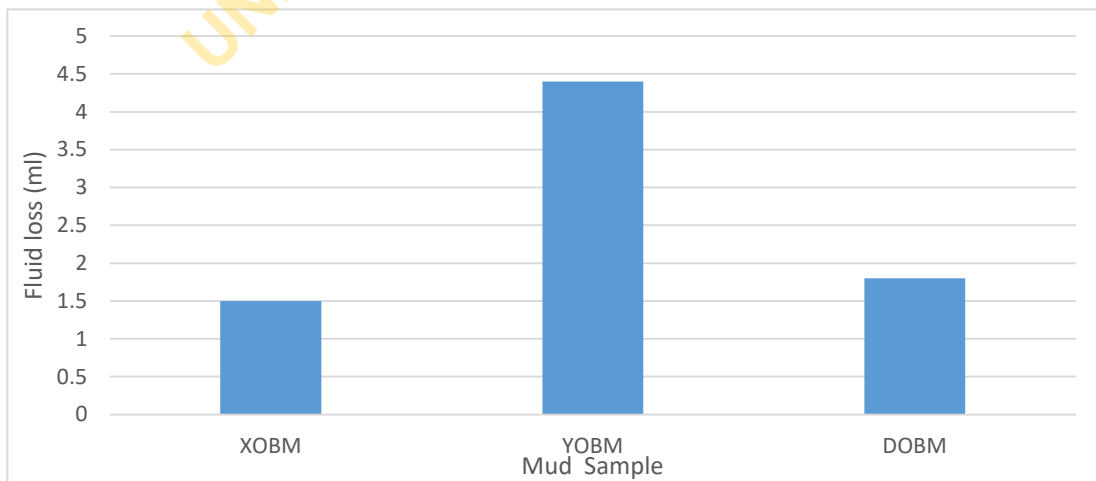


Figure 4.0: Fluid loss(ml) at 30mins for X OBM, Y OBM and DOBM**Economic Analysis:**

The required mud and cuttings generated volume were determined using the equations 7.0 and 8.0, respectively, and the result presented in the Table 4.0

Assuming an oil solid water ratio of 70:20:10

Table 4.0: Mud Volume and Volume of Cuttings Generated for the Intermediate and Production Zone

Casing Zone	Mud Volume (barrels)	Volume of Cuttings Generated (barrels)
Intermediate Zone	383.0	1094.0
Production Zone	163.0	187 .0
Total	546.0	1281.0

Cost Requirements

The cost required was calculated using the equation 9.0 and the result for each oil is as shown in the Table 5.0

Table 5.0: Oil cost per barrel (\$), Cost requirement, (\$) and Total Well cost, (\$)

OBM	Oil Cost per barrel (\$)	Cost Requirements (\$)	Total Well Cost (\$)
Y	190.80	98,505.60	14,436,395.60
X	166.95	89,395.00	\$14,427,285.00
D	103.75	129,302.50,	14,467,192.50

NET PRESENT VALUE (NPV) PROFILE**Operational parameters:**

Nominal production decline rate = 17% per year

Initial production = 500 barrels per day

Cost and Fiscal parameters:

Operating cost = \$10 per barrel

Oil price = \$40 per barrel

Discount rate = 10% per annum

Depreciation = 5 years (straight line method)

Investment split (Tangible: Intangible) = 70:30

The NPV models of the use of Y, X and D OBMs. in drilling a well in the AB1 foothills of the Alberta region in Canada is presented in the Appendix A, B and C. From the results, it is observed that the use of X OBM gave the most returns as it has the least well cost requirements and the highest NPV (Figure 1.0) this is followed by Y OBM and DOBM. The Net Present Value models of the use of Y, X, and diesel OBMs, are presented in the Appendices A, B and C, respectively. For drilling a well in the AB1 foothills of the Alberta region in Canada. From the NPV, it can be observed that the use of X OBM gives the most returns of the three mud systems as it has the least well cost requirements. Based on the

NPV values from the Figure 1.0, X OBM has the highest NPV followed by Y OBM and DOBM. Based on the discounted profit ratio Figure, (Figure 2.0), the use of X OBM gives a better investment result as more is obtained on each unit of the investment compared to when using either diesel OBM or Y OBM.

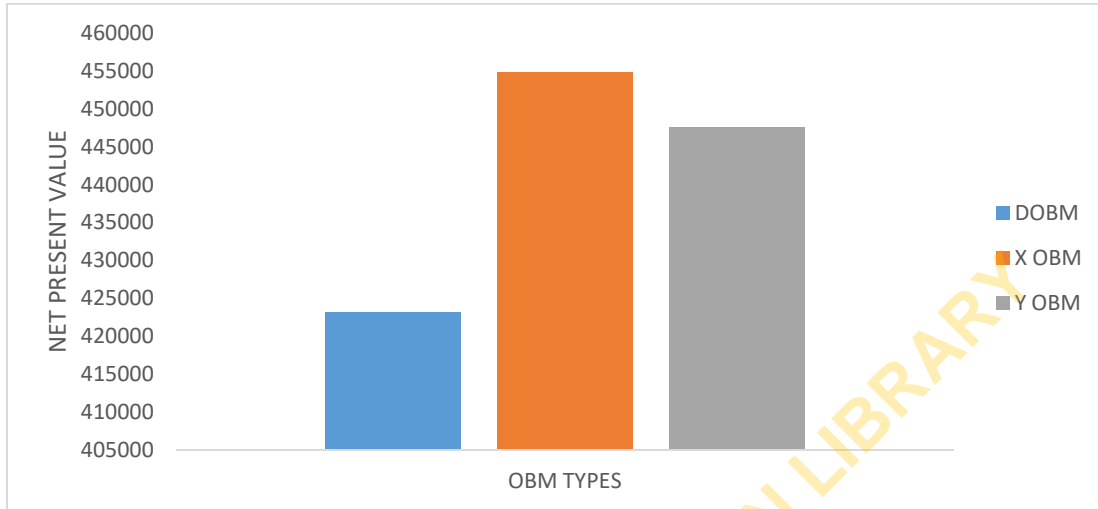


Figure 5.0: NPV profile for Y OBM, X OBM and D OBM

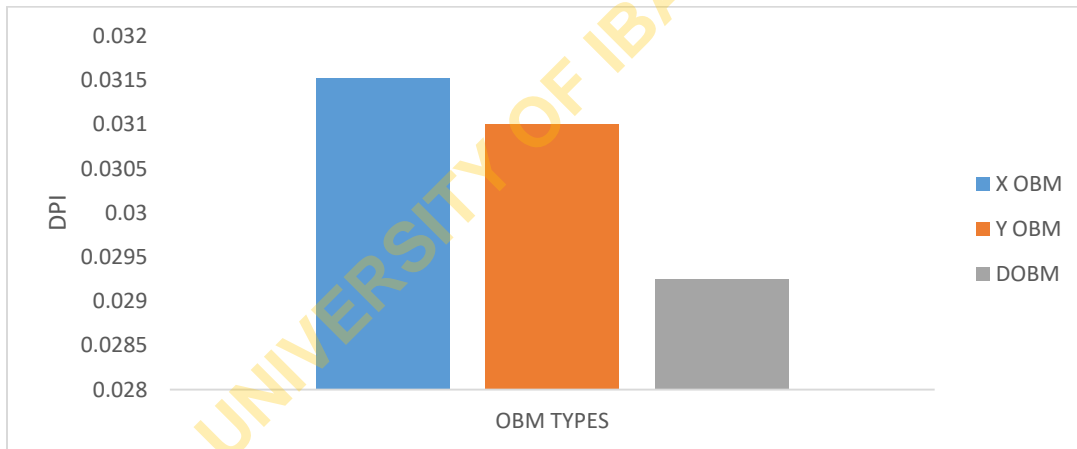


Figure 6.0: DPI values for Y OBM, X OBM and D OBM

Conclusion

From the results obtained, it was observed that the vegetable oils X and Y have the potential to be used to substitute for No. 2 diesel as base fluid in oil base mud. Although the costs of the use of the vegetable oils X and Y is higher, it will be offset when considering the cost of containment, hauling, and disposal of No. 2 diesel OBM after use. From the results of the economic analysis, it shows that the use of the X OBM has the greatest comparative cost advantage to the other mud systems, it also gives a better projected Net Present Value (NPV) and the best discounted profit to investment ratio.

Recommendations

The use of drilling fluid formulated from local materials would not only eradicate the problem arising from pollution but also provide a long-lasting socio-economic effect such as wealth and job creation, improvement on the relationship between the agricultural and energy sectors and also increase the nation's GDP

Where:

I = initial investment.

t = time (years)

CF_t = Net cash flow for each year (i.e. income less costs)

d = drill pipe id (inches)

D = Depth (feet),

Φ = formation porosity

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Appendix A

Year	Daily Production	Annual production	Oil Price	Gross Annual Revenue	Royalty \$	Net Revenue
0		0	40	0.00	0.00	0.00
1	500.00	182500	40	7300000.00	1350500.00	5949500.00
2	415.00	166506.04	40	6660241.56	1232144.69	5428096.87
3	344.45	138200.01	40	5528000.49	1022680.09	4505320.40
4	285.89	114706.01	40	4588240.41	848824.48	3739415.93
5	237.29	95205.988	40	3808239.54	704524.31	3103715.22
6	196.95	79020.97	40	3160838.82	584755.18	2576083.64
7	163.47	65587.405	40	2623496.22	485346.80	2138149.42
8	135.68	54437.547	40	2177501.86	402837.84	1774664.02
9	112.61	45183.164	40	1807326.54	334355.41	1472971.13
10	93.47	37502.026	40	1500081.03	277514.99	1222566.04
11	77.58	31126.681	40	1245067.26	230337.44	1014729.81
12	64.39	25835.146	40	1033405.82	191180.08	842225.75

Intangible Investment	Tangible Investment	Total Investment	Depreciation	Operating Cost, \$/bbl	Annual Operating Expense
4330909.05	10105454.46	14436363.51		10	0.00
			2021090.89	10	1825000.00
			2021090.89	10	1665060.39
			2021090.89	10	1382000.12
			2021090.89	10	1147060.10
			2021090.89	10	952059.88
				10	790209.70
				10	655874.05
				10	544375.47
				10	451831.64
				10	375020.26
				10	311266.81
				10	258351.46

Before Tax Income	Tax	After Tax Income	Net Flow Cash	Cumulative Net Flow Cash	DCF @ 10 %	NPV @ 10 %
-4330909.05	-1082727.26	-3248181.79	-13353636	-13353636.2	-13353636.25	
2103409.11	525852.28	1577556.83	3598647.72	-9754988.52	3271497.93	
1741945.59	435486.40	1306459.19	3327550.08	-6427438.44	2750041.391	
1102229.39	275557.35	826672.04	2847762.93	-3579675.51	2139566.44	
571264.94	142816.23	428448.70	2449539.6	-1130135.91	1673068.504	
130564.45	32641.11	97923.34	2119014.23	988878.315	1315741.118	447595.0263
1785873.93	446468.48	1339405.45	1339405.45	2328283.76	756059.4577	
1482275.36	370568.84	1111706.52	1111706.52	3439990.29	570481.2272	
1230288.55	307572.14	922716.41	922716.414	4362706.7	430454.0169	
1021139.50	255284.87	765854.62	765854.623	5128561.32	324797.1218	
847545.78	211886.45	635659.34	635659.337	5764220.66	245074.1919	
703463.00	175865.75	527597.25	527597.25	6291817.91	184919.6175	
583874.29	145968.57	437905.72	437905.718	6729723.63	139530.2569	

Appendix B

Year	Daily Production	Annual production	Oil Price	Gross Annual Revenue	Royalty \$	Net Revenue
0		0	40	0.00	0.00	0.00
1	500.00	182500	40	7300000.00	1350500.00	5949500.00
2	415.00	166506.04	40	6660241.56	1232144.69	5428096.87
3	344.45	138200.01	40	5528000.49	1022680.09	4505320.40
4	285.89	114706.01	40	4588240.41	848824.48	3739415.93
5	237.29	95205.988	40	3808239.54	704524.31	3103715.22
6	196.95	79020.97	40	3160838.82	584755.18	2576083.64
7	163.47	65587.405	40	2623496.22	485346.80	2138149.42
8	135.68	54437.547	40	2177501.86	402837.84	1774664.02
9	112.61	45183.164	40	1807326.54	334355.41	1472971.13
10	93.47	37502.026	40	1500081.03	277514.99	1222566.04
11	77.58	31126.681	40	1245067.26	230337.44	1014729.81
12	64.39	25835.146	40	1033405.82	191180.08	842225.75

Intangible Investment	Tangible Investment	Total Investment	Depreciation	Operating Cost \$ / bbl	Annual Operating Expense
4328176.71	10099078.	14427255.69		10	0.00
			2019815.80	10	1825000.00
			2019815.80	10	1665060.39
			2019815.80	10	1382000.12
			2019815.80	10	1147060.10
			2019815.80	10	952059.88
				10	790209.70
				10	655874.05
				10	544375.47
				10	451831.64
				10	375020.26
				10	311266.81
				10	258351.46

Before Tax Income	Tax	After Tax Income	Net Cash Flow	Cumulative Net Cash Flow	DCF @ 10 %	NPV @ 10 %
-						
4328176.71	-1082044.18	-3246132.53	-13345212	-13345211.5	-13345211.51	
2104684.20	526171.05	1578513.15	3598328.95	-9746882.56	3271208.136	
1743220.68	435805.17	1307415.51	3327231.31	-6419651.26	2749777.941	
1103504.48	275876.12	827628.36	2847444.16	-3572207.1	2139326.941	
572540.03	143135.01	429405.03	2449220.82	-1122986.28	1672850.777	
131839.54	32959.89	98879.66	2118695.45	995709.178	1315543.184	454811.3546
1785873.93	446468.48	1339405.45	1339405.45	2335114.63	756059.4577	
1482275.36	370568.84	1111706.52	1111706.52	3446821.15	570481.2272	
1230288.55	307572.14	922716.41	922716.414	4369537.56	430454.0169	

Economics of Local Materials as Base Fluids in The Formulation of an Oil Based Mud

1021139.50	255284.87	765854.62	765854.623	5135392.19	324797.1218	
847545.78	211886.45	635659.34	635659.337	5771051.52	245074.1919	
703463.00	175865.75	527597.25	527597.25	6298648.77	184919.6175	
583874.29	145968.57	437905.72	437905.718	6736554.49	139530.2569	

Appendix C

Year	Daily production	Annual production	Oil Price	Gross Annual Revenue	Royalty \$	Net Revenue
0		0	40	0.00	0.00	0.00
1	500.00	182500	40	7300000.00	1350500.00	5949500.00
2	415.00	166506.04	40	6660241.56	1232144.69	5428096.87
3	344.45	138200.01	40	5528000.49	1022680.09	4505320.40
4	285.89	114706.01	40	4588240.41	848824.48	3739415.93
5	237.29	95205.988	40	3808239.54	704524.31	3103715.22
6	196.95	79020.97	40	3160838.82	584755.18	2576083.64
7	163.47	65587.405	40	2623496.22	485346.80	2138149.42
8	135.68	54437.547	40	2177501.86	402837.84	1774664.02
9	112.61	45183.164	40	1807326.54	334355.41	1472971.13
10	93.47	37502.026	40	1500081.03	277514.99	1222566.04
11	77.58	31126.681	40	1245067.26	230337.44	1014729.81
12	64.39	25835.146	40	1033405.82	191180.08	842225.75

Intangible Investment	Tangible Investment	Total Investment	Depreciation	Operating Cost, \$/bbl	Annual Operating Expense
4340144.44	10127003.70	14467148.14		10	0.00
			2025400.74	10	1825000.00
			2025400.74	10	1665060.39
			2025400.74	10	1382000.12
			2025400.74	10	1147060.10
			2025400.74	10	952059.88
				10	790209.70
				10	655874.05
				10	544375.47
				10	451831.64
				10	375020.26
				10	311266.81
				10	258351.46

Before Tax Income	Tax	After Tax Income	Net Flow Cash	Cumulative Net Flow Cash	DCF @ 10 %	NPV @ 10 %
-4340144.44	-1085036.11	-3255108.33	-13382112	-13382112	-	
2099099.26	524774.82	1574324.45	3599725.18	-9782386.84	13382112.03	
1737635.74	434408.94	1303226.81	3328627.54	-6453759.3	3272477.441	
1097919.54	274479.88	823439.65	2848840.39	-3604918.9	2750931.855	
566955.09	141738.77	425216.32	2450617.06	-1154301.85	2140375.953	
126254.60	31563.65	94690.95	2120091.69	965789.844	1673804.425	
					1316410.137	423203.6738

1785873.93	446468.48	1339405.45	1339405.45	2305195.29	756059.4577	
1482275.36	370568.84	1111706.52	1111706.52	3416901.82	570481.2272	
1230288.55	307572.14	922716.41	922716.414	4339618.23	430454.0169	
1021139.50	255284.87	765854.62	765854.623	5105472.85	324797.1218	
847545.78	211886.45	635659.34	635659.337	5741132.19	245074.1919	
703463.00	175865.75	527597.25	527597.25	6268729.44	184919.6175	
583874.29	145968.57	437905.72	437905.718	6706635.16	139530.2569	

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